

MARKED UP VERSION OF AMENDED CLAIMS

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2. (Amended)      The [P] process [according to] of claim 1, wherein the gaseous fraction obtained in the stripping section is supplied directly to the absorber section.

3. (Amended)      The [P] process [according to any one] of claim[s] 1 [-2], wherein  
10 the higher boiling liquid fraction obtained in the absorber section is supplied to step (a).

4. (Amended)      The [P] process [according to any one] of claim[s] 1 [-3], wherein the stripping section and the absorber section are combined in one distillation column.

15 5. (Amended)      The [P] process [according to] of claim 4, wherein the hydrocarbon rich liquid fraction obtained in step (a) is fed to a position in the distillation column above the feed inlet of the hydrocarbon rich gaseous fraction obtained in step (b).

6. (Amended)      The [P] process [according to any one] of claim[s] 1[-5], wherein  
20 the hydrogen separation selectivity of the membrane separation in step (b) is greater than 20, wherein the hydrogen separation selectivity is defined as the permeability ratio of hydrogen over methane. .

7. (Amended)      The [P] process [according to any one] of claim[s] 1[-6], wherein  
25 the methane separation selectivity of the membrane separation in step (b) is greater than 5, wherein the methane separation selectivity is defined as the permeability ratio of methane over propane.